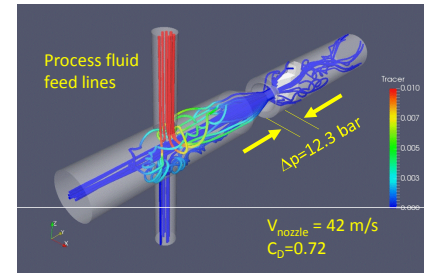
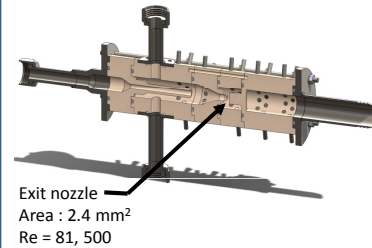


Unilever is interested in the application of CFD for a number of process areas:
Newtonian fluids (i.e. Backwashing)
Non-Newtonian (structured) liquids (gels, emulsions etc. laminar or turbulent)

3 non-Newtonian viscosity models have been implemented into **CODE_SATURNE**

$$\begin{aligned} \tau &\propto S && \text{Newtonian} \\ \tau &\propto |S|^{n-1} S && \text{Power law} \\ \tau - \tau_0 &\propto |S|^{n-1} S && \text{Herschel-Bulkley} \\ \tau &\propto (a + b|S|^{n-1}) S && \text{Sisko} \end{aligned}$$

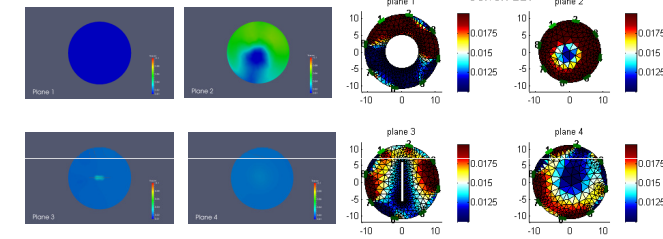
Static inline mixer



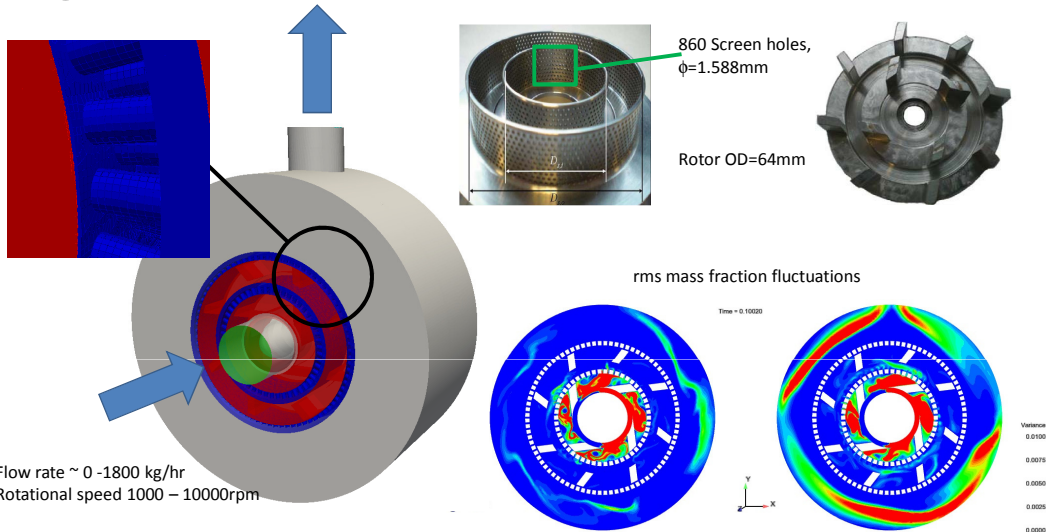
Downstream mixing

URANS: k-ε turbulence model
(2.1 million cells)

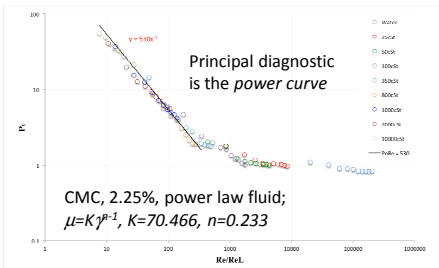
Typical ERT results (P. Martin, (UoM))



High shear batch mixer



Flow rate ~ 0 -1800 kg/hr
Rotational speed 1000 – 10000rpm



- These simulations (2D & 3D) use *Sliding meshes*
 - Important to get laminar *extensional* and *folding* flow
 - 2D : 180x10³ cells on 64 cores, 12.5Hrs per simulated revolution (CSF)
 - 3D : 7.5x10⁶ cells on 960 cores, 8.5 Hrs per simulated revolution (HPC)

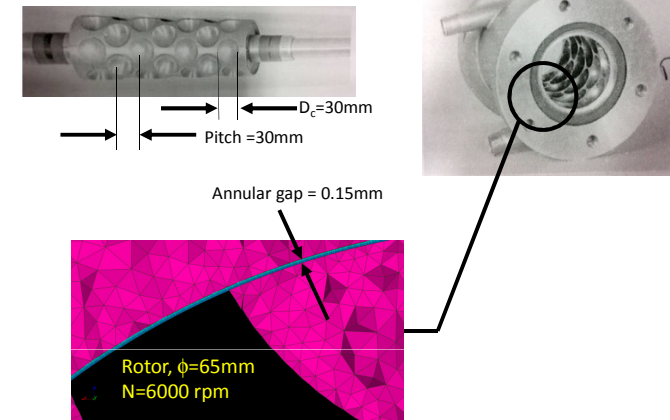
- Where turbulent, (curvature compensated) SST and SSG models are used
- Modified wall treatments

$$v = K \dot{\gamma}^{n-1} \frac{U}{u_\tau} = A(n) \ln(y^+) + B(n) \quad (y^+)^{2-n} = \frac{u_\tau^{2-n} y}{K}$$

Cavity transfer mixer (CTM)

Mixing comes from movement between cavities
Flow tortuosity & high shear improves mixing

Goal: maximize mixing, minimize Δp, power and remove leak path.



Model : k-ε turbulence model with rotation correction
3D : 2.86x10⁶ cells on 144 cores, 9Hrs per simulated revolution

Validation:

Pilot scale CTM (CEAS, UoM)

Rotor φ = 65mm
Cavity φ = 30 mm
Annulus = 0.15mm
N = 100 Hz, Q = 100 l/h
60 % g/w solution
Re_{CAV} = 66,450

Parametric studies: Mixing,
Power/ΔP vs. N, Q

